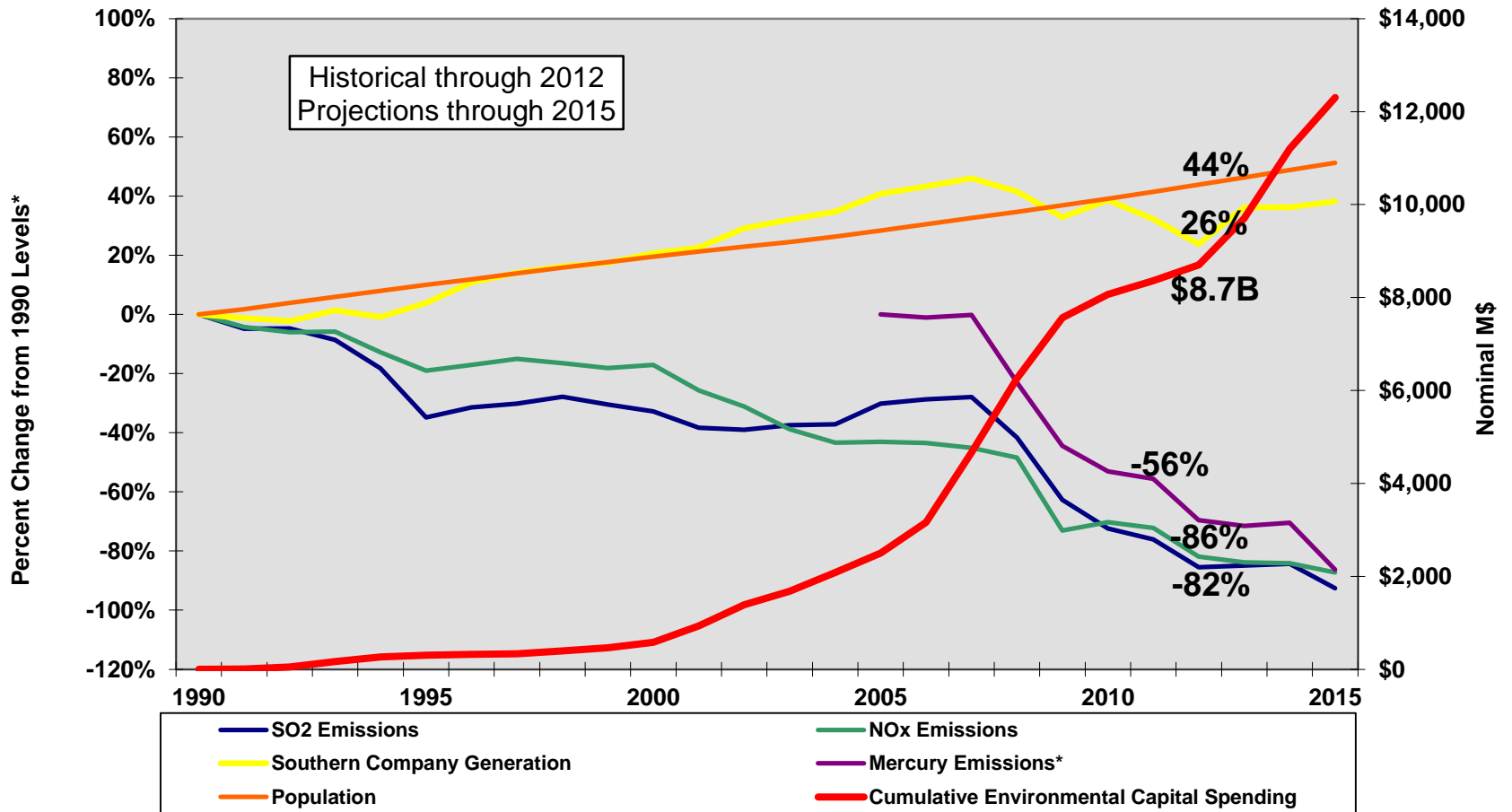


NOx Reduction Technologies

M. Brandon Looney, P.E.



Emissions and Environmental Capital Expenditures Historical and Projected*



* For Mercury, percent change from 2005.

NO_x Reduction

Alternatives

- Low NO_x burners (LNB)
- LNB + Overfire Air (OFA)
- Simulated OFA (Burners Out Of Service)
- Coal switching
- Natural Gas (general & seasonal)
- Reburn
- Selective Catalytic Reduction (SCR)
- Selective Non-Catalytic Reduction (SNCR)
- Repowering
- Retirement

NOx Burner Goals

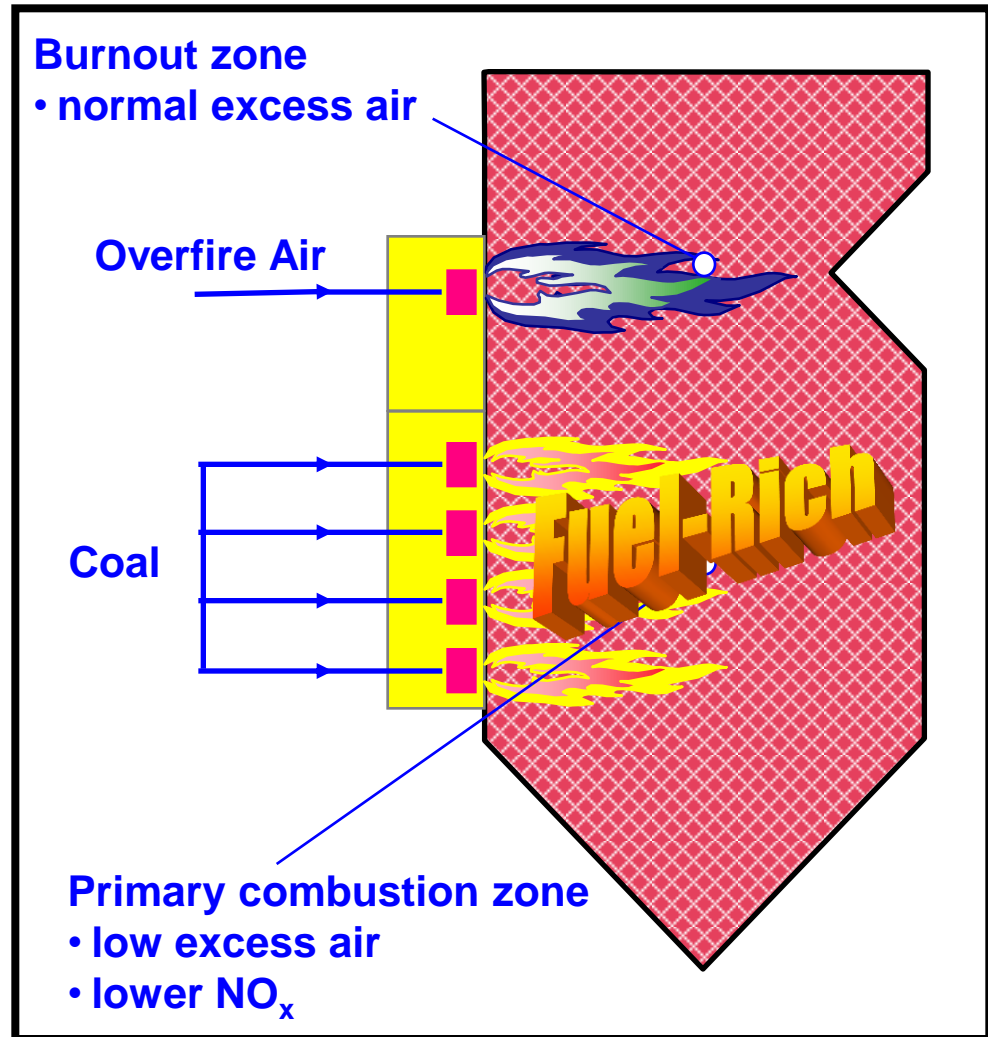
- Control mixing of fuel and air in the furnace to reduce NOx emissions while:
 - efficiently burning the fuel
 - maintaining steam flow, temperatures and pressures
 - not compromising reliability
 - limiting impacts on maintenance.

NOx Reduction in Low NOx Burners

- The three T's of Low NOx Combustion
 - Time
 - Temperature
 - Turbulence
- Time in the Low NOx burner is extended by increasing the initial flame length **while maintaining early ignition**
- Low NOx burners reduce peak flame temperatures
- Turbulence is controlled by imparting swirl on the various air streams which in turn controls the fuel/air mixture

Overfire Air

- Carbon likes O_2 more than nitrogen
- 10 to 30% of the total combustion air injected above the top burner level
- Deprive main flame of oxygen
- Fuel nitrogen converted to N_2
- Can be used with LNB to increase NO_x reduction by 10 to 25%



Southern Company LNB Efforts

- Two DOE Advanced Combustion Techniques demonstrations (wall fired and tangentially fired application)
- One additional wall fired demonstration as an EPRI collaboration.
- Demonstration of advanced on-line optimization systems.
- Approximately 35 commercial installations of Low NO_x combustion systems.
- Emission range from 0.20 to 0.45 lb/MMBtu

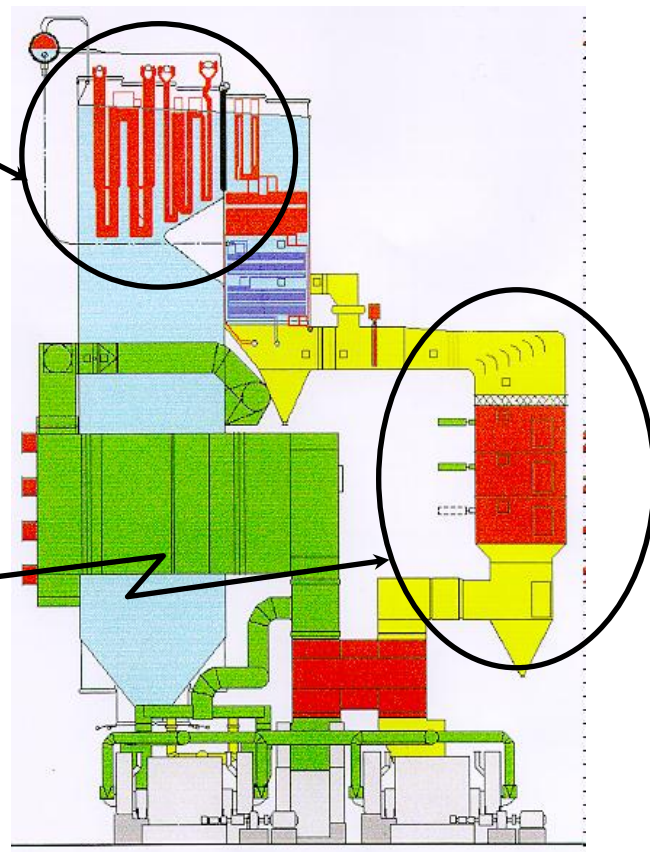
SCR System Overview

Selective Non-Catalytic Reduction

- 1600 - 2000 °F
- 15 - 40% Reduction
- >5 ppm NH₃ Slip
- \$8 - \$20/kW Capital Cost
- \$800 - \$2500/ton Levelized Cost

Selective Catalytic Reduction

- 550 - 750 °F
- 50 - 90% Reduction
- <5 ppm NH₃ Slip
- \$80 - \$150/kW Capital Cost
- \$1500 - \$5300/ton Levelized Cost



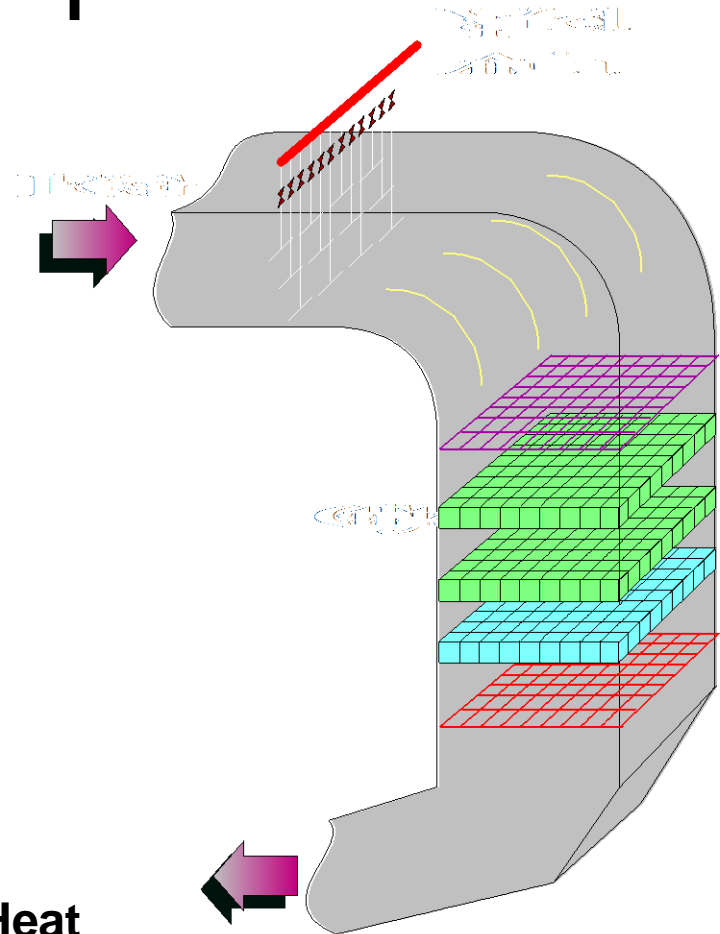
Southern Company SNCR Efforts

- Initial demonstration at APC Plant Barry
- Nine commercial installations
- Typical performance 15% - 20% NO_x reduction



SCR Principles of Operation

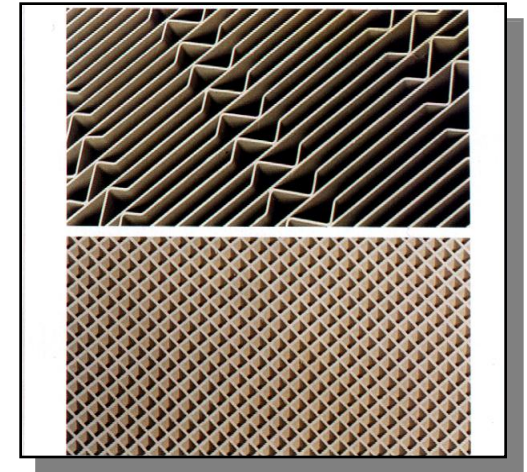
- The SCR process works by injecting ammonia into flue gas as a reagent for reducing nitrogen oxides of NO
- Flue gas passes over a fixed bed catalyst installed in a reactor
- Ammonia reacts with nitrogen oxides on the catalyst surface to form molecular nitrogen and water



Catalyst Performance

Requirements

- High activity over a wide temperature range
- High selectivity (low SO_2/SO_3 conversion rate)
- Thermal stability
- Mechanical stability
- Low pressure loss
- Recyclable / disposable
- Resistant to deactivation mechanisms



Southern Company SCR Efforts

- Pilot SCR demonstration at Gulf Power Plant Crist
- Commercial installation at SEI Birchwood Plant
- Approximately 20 commercial installations to date
- Emission less than 0.01 lb/MMBtu



Southern Company SCR Philosophy

- SCR Emission Performance
 - 85% NO_x Reduction
 - 2 ppm NH₃ Slip with NO_x and Slip Distribution
 - 16,000 Hour Catalyst Life
 - 1% SO₂ to SO₃ Oxidation (maximum)
 - Pressure Drop Determined on Plant by Plant
- Use Combination of Cold Flow and CFD Modeling
- Maximize Use of Modularized Design & Construction
- Volume Procurement of SCR Components

Major SCR Issues

- Catalyst Selection and Catalyst Management
- Flyash and Popcorn Ash Pluggage
- Boiler Turndown and Dispatch Restrictions
- SO₂/SO₃ Oxidation Rate
- Understanding Hg Oxidation



QUESTIONS ?